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Task III-Data Dump

15 November 1974

High Performance

N204/Amine Elements - "Blowapart"

Contract NAS 9-14186

_Report 14186-DRL-3-1

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(NASA-CR-141480) HIGH PERFORMANCE N204/AMINE ELEMENTS: BLOWAPART (Aerojet Liquid Rocket Co.) 43 p HC \$3.75 CSCL 21I

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Aerojel Liquid Rockel Company

CESTS OF BUILDING

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INTRODUCTION AND SUMMARY

I

The objective of this program is to develop an understanding of the mechanisms controlling hypergolic propellant blowapart and with that understanding develop a model containing the parameters controlling blowapart which will aid the design of stable high performing injectors. The mechanisms will-be defined through test and analysis of subscale injectors using principally N_2O_4/MMH propellants and injectors and test conditions representative of the OME and Space Tug applications.

The program consists of four tasks. The objectives of the Task I effort are; to critique all existing models relating to blowapart, to summarize and review all associated experimental data and formulate updated models. The Task II effort consist of preparing a detailed program plan. The objectives of the Task III effort are to define the mechanisms governing blowapart through the design, fab, test and analysis of single element injectors. The objectives of Task IV are to verify the mechanisms governing blowapart and to extend RSS mapping to other injector elements.

This document summarizes the work performed during the Task III effort. Results of the Task I model review effort indicated that neither of the two existing blowapart models (JPL model and ALRC model) adequately describes RSS nor correlates the experimental data. New data correlations were developed that show the parameters exhibiting a controlling influence over blowapart are the chamber pressure, orifice diameter, and propellant temperature. Four regimes of reactive impingement were defined:

- o Mixing.
- Popping (cyclic blowapart),

- Low pressure separation (P∠ 300 psia), ...
- e High pressure separation ($P_c > 300 \text{ psia}$)

The objectives of Task III testing were to concentrate on the high pressure mode of RSS, to verify the model concepts, and to map regions of RSS for the unlike doublet injector element. High speed color movi were used to verify operating modes. Tests with two unlike doublet elements of differing impingement lengths verify the high pressure model analytical results in that recirculation gas heating does not control RSS and that other mechanisms are operative.

Impingement point temperature measurements indicate the existence of two modes of high pressure RSS which are depertent. The pressure, temperature, and velocity. High speed color movies show that is degree of RSS increases gradually with increasing pressure and increasing fuel temperature.

.II <u>CONCLUSIONS</u>

The conclusions drawn from the Task III testing are summarized in Table I.

III TEST RESULTS

The two unlike doublet injector elements shown in Figure 1, were tested over the range of parameters listed in Table II to determine their influence on RSS. The injector, test chamber, and test setup are described in detail in Section V.

. The test objectives and results are summarized in Table III. A detailed test condition log was maintained and included as Table IV. The test data are stored in a computer data file for easy manipulation and correlation. A listing of the reduced data is shown in Table V.

The objectives of the first series of tests (#101-106) were to verify proper test stand operation and to check the photographic equipment. The tests showed that the backlighting intensity was too bright and that the test stand functioned as required. Examination of the movie pictures showed all of the tests to be separated. Separation is defined as the appearance of unmixed oxidizer in the spray field evidenced by clouds of dark brown NO₂. Although density gradients between the cold window purge gas and the hot combustion gas obscures detail in the impingement zone at the higher pressure, the spray field operating mode is readily discernible.

The backlight was modified prior to the next test series to improve photography. A sheet of polorized filter paper and a sheet of ground glass were placed between the Fresnel lense and the test chamber to reduce the backlighting intensity and to eliminate parallel light from the quartz lamp.

The next series of tests (#107-111) were run at lower pressures to determine the pressure limit of RSS. The onset of RSS was found to occur

between 100 and 150 psia. The recirculation gas model developed in Task I had predicted separation at about 400 psia with MMH. RSS was found to gradually worsen with increasing pressure. The density gradients were still visible but their intensity was found to decrease with pressure. Good, clear pictures were obtained at the lower pressures (100-200 psi).

the influence of fuel vapor pressure on RSS. The hot gas recirculation model had predicted that A-50 would separate at 500 psia as compared to 400 psia for MMH. The data shows A-50 to separate at about 200 psia as compared to about 150 psia for the MMH. The increase in separation severity with pressure is readily apparent in Figure 2 which shows a series of single movie frames from successive tests at increasing chamber pressures. Test No. 117 was run at a lower injection velocity to determine its influence on RSS. The movie film shows notably less separation at the lower velocity (88 ft/sec) than at the nominal velocity (125 ft/sec). Subsequent temperature probing indicates the same trend.

The next series of tests (no. 124-132) were run with the short impingement length doublet to determine the influence on RSS. The Task I model had indicated that RSS should depend on impingement length. The movie data do not show any discernible difference in separation characteristics between the long impingement (0.160 in.) and the short impingement (0.060 in.) doublet elements.

Test Numbers 134-138 were run with heated fuel over the pressure range of 100-250 psia. The movies show a pronounced worsening of separation with increased fuel temperature. This influence is demonstrated by the movie frames shown in Figure 3. Also shown in Figure 3, is the thermocouple used

to probe the impingement point in the subsequent set of tests. The onset of separation was found to occur at 100 psia with 200°F MMH.

The final test set (No. 139-152) were run with ambient temperature propellants and the thermocouple probe mounted as shown in Figure 3. Initially, a 0.010 in. dia thermocouple was used, however, it lacked sufficient mechanical strength to remain in a fixed position. It was discarded for a more rigid 0.020 in. dia thermocouple. The movies indicate some disruption of the impingement by the thermocouple particularly at the lower velocity conditions, however, the temperature data are reasonably consistent and orderly. The temperature probing technique appears to offer significant quantitative data and therefore will be improved for the Task IV testing.

The impingement point temperature was found to depend on the chamber pressure and the propellant velocity as shown in Figure 4. These influences appear to be accounted for by adding the propellant stream dynamic head to the chamber pressure as shown in Figure 5. Also included in Figure 5 are the saturation temperature lines for $N_2 O_4$ and MMH. It appears that separation, as determined visually from the movies, occurs when the impingement point temperature exceeds the $N_2 O_4$ saturation temperature and that there is a change in mode of separation when the temperature exceeds the MMH saturation temperature.

The impingement process was observed to be cyclic in nature in both the mixed and separated modes. The characteristic frequencies were the same in both modes, suggesting that it is characteristic of the ligament shedding process. Energetic cyclic blowapart (i.e., popping) was not observed on any of the tests. The Task I data correlations would indicate that none should

occur over the range of variables tested.

IV MODEL CORRELATIONS

The RSS data for both MMII and A-50 fuels were plotted on the pressure versus temperature scales as shown in Figure 6 for comparison with the Task I data correlations. It is noted that the A-50 separates at a higher pressure than the MMII and that the pressure at which MMH separates decreases with increasing fuel temperature. The N_2H_4 data of Zung (Ref. 1) shown in Figure 7 does not reflect the influence of inlet temperature. Testing with N_2H_4 under similar conditions is recommended to confirm the differences.

Listed in Table VI are the predicted and measured RSS pressure limits for MMH and A-50 at ambient temperature. Also included is Zung's N_2H_4 data for reference. The pressure limits were predicted on the basis of the recirculation gas heating model developed in Task I. The model states that separation should occur at the pressure corresponding to the fuel vapor pressure at 450°F, the vapor phase decomposition temperature. It is seen that the pressure levels do not agree and that the trend in fuel type is correct for MMH and A-50 but not for N_2H_4 . In view of this and the fact that the analytical calculations had indicated insufficient heating, the hot gas recirculation model does not appear valid.

The correspondence between heat release rates and the onset of RSS would seem to indicate a dependence on propellant reactivites as shown in Table VII.

The model concepts developed on Task I were based on the complex reaction mechanisms of hypergolic fuels. A summary of these concepts is included

in Figure 8 for reference in discussing the temperature probe results. The temperature data of Figure 5 shows two modes of RSS as evidenced by a step change in temperature. The temperature discontinuity is indicative of a change in reaction mechanism as suggested by the popping regime mechanism (Figure 8). It is believed that low enthalpy surface reactions predominate at the lower pressure conditions. These reactions heat the propellants to their saturation temperatures and when the fuel saturation temperature is exceeded, the reaction switches to a high enthalpy gas phase reaction. The onset of visual separation occurs when the temperature exceeds the $N_2 O_4$ saturation temperature.

A surface controlled reaction would be expected to be primarily a function of the propellant interfacial surface area which is expected to be related to propellant stream turbulence level or Reynold number. As shown in Figure 9 there is a dependence of ΔT_i on R_e up to the point of transition. A free jet may also experience some self atomization prior to impingement thus influencing effective surface area. The self atomization is characterized by the ratio of aerodynamic to surface tension forces as described by the Weber number. The impingement point temperature rise is plotted versus the fuel and the exidizer Weber number in Figure 10. There appears to be some dependence of ΔT_i on Weber number. It is noted that the temperature transition occurs beyond the critical Weber No. which signifies the enset of self atomization and increased surface area.

On the basis of these results a model of surface controlled reactions is in the process of being developed but requires additional data which will be obtained during the Task IV testing. Computerized data correlations of all the Task I data will be developed on the basis of these model results.

TEST HAPPWARE AND SETUP

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A. Test Apparatus

The test apparatus consists of a test chamber equipped with transparent viewing ports and removable injectors and nozzles as shown in Figure 11.

1. Test Chamber

The test chamber is machined from a 4-inch square x 6-inch long block of 304 CRES. The combustion chamber section is 4 inches long, to which a 2 in. L* spacer is bolted to increase the combustion zone length to 6 inches. The block is bored to provide a 2.75 inch diameter combustion chamber. Four circular quartz windows are provided to facilitate photography and to allow flexibility in photographic lighting of the combustion process. The windows are 1/2 inch thick to provide a safety margin for 1000 psia operation. The flat quartz windows are sandwiched between durabula gaskets for cushioning against ignition shocks and uneven loading. A silicon "O" ring provides sealing on the window periphery. Quartz provides good propellant compatibility and well defined optical properties.

An inert gas (GN_2) film purge is provided to prevent obscuring the view by propellant spray impingement on the windows. The gas purge flow is injected through four inlets into an annular manifold. The gas is directed from the manifold through an annular gap and made to flow around the periphery of the chamber wall. The gas passages are sized such that the GN_2 is injected into the chamber at 50 ft/sec at 300 psia chamber pressure to minimize mixing with the propellant spray and combustion gas.

Provision is mode for mounting both high and low frequency response pressure transducers and thermocouples as required. The nozzles consist of removable copper associal brilled to provide the desired operating pressures.

2. Injectors

The injector body is a cylindrical shaped "piston" designed to fit into the purge ring located at the forward end of the chamber. The injector is held in the purge ring by Allen head screws. A silicon rubber 0-ring seals the injector to the purge ring.

The injector consists of a main body with brazed-on inly leaves. Two injector patterns are incorporated in one body as shown in Figure 1 to reduce fabrication costs. The element design parameters are shown in Figure 1. The orifice L/D's are 24/1 with rounded inlets to provide controlled hydraulics. The injectors are made of 304 CRES to permit braze assembly and provide dimensionally stable orifices.

The injector orifices were flow tested prior to hot fire testing to verify impingement and pattern accuracy. The flow data are plotted in Figure 15.

A high frequency response Kistler pressure transducer mounting port was provided as shown in Figure 1 to measure impingement point disturbances.

B. Test Facility Setup

The test apparatus was setup in the Research Physics Laboratory
Test Bay 2 shown in Figure 13.

A schematic of the propellant system used is shown in Figure 14. Propellant (MMH/A-50/NTO) is stored in 50-gallon, 3000-psi run vessels. Gaseous nitrogen pressurization of these systems was used to provide controlled run conditions over a wide range of injector and chamber pressures.

Propellant conditioning was provided by installing in-line heat exchangers immediately upstream of the thrust chamber valves. A hot water circulation type temperature conditioning system was used to provide independent conditioning of the ox and fuel to temperatures from ambient to 300°F.

A separately regulated GN₂ Supply was used to provide test chamber back pressure as well as provide window purge for the chamber viewports.

C. Instrumentation

lligh speed color photographs of the spray field were taken with the photographic equipment shown in Figure 13. Pictures were taken at 8000 pictures per second (1.25 place exposure) and at 400 PPS (25 place exposure) with a Hycam Model 41-0004 high speed camera. Four hundred foot rolls of Ecktachrome EF No. 7242 film were used which allows approximately 0.6 sec. of constant speed frame rate at 8000 PPS and approximately 30 sec. constant speed 0 440 PPS.

Lighting of the spray field was accomplished with the use of three 1000-watt quartz iodine lamps focused with Fresrel lenses. One lamp' was used to backlight the spray area with the second and third lamps used as top and front lighting to provide spray detail and definition.

High frequency and low frequency instrumentation listed in Tables VIII and IX were used in the locations shown in the schematic of Figure 15.

Low frequency response test parameters were recorded on a Consolidated Electrodynamics Corporation's direct writing oscillograph. The high frequency response data were recorded on a Sangamo Model 3564 analog tape recorder.

The operating point data indicated in Table IX were digitized and stored in the on-line HP 2100 A Computer/Real Time process controller for "quick look" test review.

REFERENCES

Zung, L. B., "Hypergolic Impingement Mechanisms and Criteria for Jet Mixing or Separation", presented at the 6th ICRPG Liquid Propellant Combustion Instability Conference, 9-11 September 1969

Task III - Definition Of Coverning Mechanisms Conclusions

RSS SEVERITY INCREASES WITH

PRESSURE

FUEL TEMPERATURE

PROPELLANT VELOCITY

RSS DEPENDS ON FUEL

• MMH > A-50

RSS NOT DEPENDANT ON IMPINGEMENT LENGTH

RECIRCULATION GAS MODEL INVALID

RSS OCCURS IN TWO MODES

• LOW ENTHALPHY REACTION (Tr > T; > To)

HIGH ENTHALPHY REACTION, (T. > T.) sat

Task III - Definition Of Governing Mechanisms Test Variables

PRESSURE

• 100 - 1000 PSIA

PROPELLANT TEMPERATURE

\$02·

• 2000F

VAPOR PRESSURE

· A-50

· MMH

IMPINGEMENT LENGTH

• 0.160 in.

• 0.060 in.

Task III - Definition Of Coverning Mechanisms Test Objectives & Results

		SEP.	20	8	BLE	PSI	13
	RESULTS	ALL SHOWED SEP.	SEP ABOVE 150 PSI	SEP ABOVE 200 PSI	NO DISCERNIBLE DIFFERENCE	SEP AT 100 PSI	IMPING. PT. TEMPERATURE VELOCITY & PRESSURE DEPENDANT
	RES	ILL SH	SEP AB	SEP AB	NO DISCERN DIFFERENCE	SEP AT	IMPING. PT. TEMPERATURE VELOCITY & PRESSURE DEPENDANT
NO.	STS	9	2		6	in .	4
Ī	凹		Ţ	12			
٥	(PSIA)	300-1000	100-300	100-1000	100-1000	100-250	100-1000
	9	300-	-001	901	90	100	92
<u>_</u>	(F)	AMB	AMB	AMB	AMB	200	AMB
		A	A	A	A	2	4
۲°	(P)	AMB	AMB	AM3	AMB	AMB	AMB
					.;		
	CTOR	LONG IMPING.	LONG IMPING.	LONG IMPING.	SHORT IMPING.	LONG IMPING.	LONG IMPING.
	INJECTOR	ONG II	ONG II	0NG 11	HORT	ONG I	ONG I
		2		_	S	-	-
	اب			0		_	_
	PIE	MMH	MMH	A-50	MMH	HMM .	MM
			SE		x	Z	ENT .
	IVE	STS	RES SU SS	APOR FECT	FFORT	FFECT URE 0	RATUR
	BJECT	UT TE	INE P	INE V RE EF	INE E	INE E	TEMPE
	TEST OBJECTIVE	CHECKOUT TESTS	DETERMINE PRESSURE LIMIT FOR RSS	DETERMINE VAPOR PRESSURE EFFECT ON RSS	DETERMINE EFFORT OF IMPING. LENGTH ON RSS	DETERMINE EFFECT OF TEMPERATURE ON RSS	MEASURE IMPINGEMENT POINT TEMPERATURE
	1-	C	0-1	000	000	000	2.4

TABLE IV - TEST LOG

HIGH PERFORMACE N₂O₄/ARINE ELEMENTS
TEST CONDITION LOG

	1													
	Rerarks	Long Impingment Element	Long Impingement Element	Long Impingerent Element	Long Impingment Element	Long Impingement Element	Long Impingement Ilement Poloroid Filter Paper & Ground Glass Diffuser Installed Setween Sacklite & Wiccom	Long Impingenent Element	Long Impingment Element	Long Impingement Element	Long Impingement Element	long impingement Element	Long Impingerent Element Noved camers to opposite Window 8 sided front Highting	tong Impingement Element
1 inhe	Reter W/2 N.D.F.	35	<u>10</u>	60	ž.	92	50	22	ħ	23	25	n	ä	и
	Process	Normal	Norma!	Norse?	Normal	1 Stop	ig S	Normal	Lamon	Normal	Nome	Normal	1 Stop	Mortal
	FR/Rate (PPS)	83	604	283	8000	8000	0000	99	430	600	69	8000	0008	400
	f-Stop	92	=	22	3.3	3.3	2	69	60	60	60	2	2	9.6
	DATE	10/1/74	10/1/74	10/11/74	27/1/01	10/1/74	4L/1/01	10/7/74	10/7/74	10/7/74	10/7/74	10/7/74	10/8/74	10/12/74
	F (315)	385	390	385	385	. 585	5801	385	335	582	535	185	202	185
	Por (PSIG)	385	380	385	385	282	280	335	333	282	535	185	5	185
	PN2 (PS16)	1350	1350	1350	1350	1463	1463	1350	1095	1568	1129	1350	1533	1350
	No.	0.330	0.330	0.330	0.330	0.265	0.187	0.330	0.33	0.432	0.432	0.553	0.563	0.563
	100	8	901	B	55	8	5	901	55	5	8	9	2	901
	۲۰	I	1	9	1	Į.	£	Ą	2	1	1	ı	1	£
	1-1	2	A	1	ı	I	2	4	g.	ı	2	g g	£	2
	£	1.6	1.5	1.6	1.6	5:	9.2	9:	1.6	1.6	97	1.6	2	9.7
	~	300	38	300	33	200	89	300	55	500	150	8	g .	901
	Fuel	*	3	ž.	×	¥	<u>E</u>	ž	ž	¥	ž	Ē	6-4	A-50
	10	020	220	520.	220.	23.	220.	020	020.	020.	020	020	8	020.
	Test %9.	101-27-101	-102	: :	201-	201-	ž.	701-	201-	601-	97	Ę	¥-	E.

ORIGINAL PAGE IN OF POOR QUALITY

MAN POO	RO	GE	M

1																	
REMARKS	Long Impingement	Long Impingment	Long impingement Element	Long impingerent Element	Long impingement	Long Impingment Element	Long impingement	Reduced window purge from 13X	Long Impingement Element	Repeat of 122	Increased burge flow to lost Stort impingerent Elerent	Short Impingement Element	Short Impingement Element	Short Impingement Element	Short Impingement Element	Short Impingment Element	Short Impingement Element
Light Neter W/Z N.D.F.	.91	7	2	2	*	2	z	#	2	22	2	71	2	2	z	2	22
Process	Normel	Norral	Normal	Normali	Normal	Normal	Normal	Norteal	Normel	Normal	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Step
FR/Rete (PPS)	007	603	8	004	8	89	69	8	4000	4000	69	2 23	88	603	500	604	400
f-Stop	5.6	9.6	5.6	3.6	5.6	5.6	5.6	9.6	3.3	3.3	9.5	9.6	5.6	5.6	5.6	5.6	5.6
	10/12/74	10/12/74	10/12/74	2/12/74	10/12/74	4T/2T/0T	10/12/74	27/21/01	10/12/74	10/12/74	27/31/01	10/16/74	27/91/01	\$ 7/\$1/01	10/16/74	10/16/74	10/16/74
Por Per DATE (PSIG)	235	285	335	305	385	285	1085	53	385	385	1085	282	385	305	335	582	512
POT (9339)	522	592	335	302	385	282	1085	83	385	385	Short	8	385	202	335	285	235
P _{N2} (PS15)	1129	1568	1095	1646	1350	1453	1463	1123	360	2	1663	1463	1350	1646	1095	1568	1129
No.	0.432	0.432	0.330	0.330	0.330	0.265	0.187	0.432	0.187	0.137	0.137	0.265	0.330	0.330	0.330	0.432	0.432
2	100	100	100	22	100	138	100	2	100	100	82	100	100	8	199	501	133
10	g	ı	£	1	2	2	Ĩ	2	1	1	£	2	1	£	Q.	2	\$
1	8	2	4	1	1	9	Ą	Q.	2	£	1	4	1	£	3	A	1
œ	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.5	1.6	1.6	1.6	1.6	1.6	1.6	1.6
~"	1 8	200	252	300	300	92	1000	150	300	300	1000	200	300	300	52	200	25
Fee.	A-56	A-50	4-50	A-50	4-50	A-50	A-50	4-50	A-50	A-50	£	*	Ē	Ē	₹.	\$	ž
ď	020	020	020	83.	920.	.020	020	020	020	.020	.020	020	020	920.	020	20.	020.
761 75.	00-27-114	-115	311-	7111-	.113	911-	-120	121-	221-	21-	321-	-125	-126	21-	821-	-13	-139

	Page 3 of 4	REMANS	Short Impingerent Element	Short Impingerent Element	Long Instrugement Element	Long Impingerent Element	Long Impirgement Element	Long Impingement Element	Long Impingment Element	Long Impingement Element Heater Purp Seal Walf, installed T/C @ Imping, Ft.	Long Impingerent Element		Changed I/C from 0.01" Dia. to 0.027 Dia. prior to test 142	Long Impirgement Element	Long impingement Element	Long Impingment Element	Long Impingment Element	Long Impingment Element
		N.D.F	7 .	¥		2	7	2	72	2	2	14	7	7	2	2	2	2
		Process W/2 N.D.F.	Push 1 Stop	Push 1 Stop		Push 1 Stop	Fush 1 Step	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop	Push 1 Stop
		FA/Pate (PPS)	8	4000	oto	89	83	8	8	8	60	609	8	8	8	8	400	88
		f-5top	5.6	33	Still Photo	5.6	3.6	9.6	5.6	9.9	9.6	5.6	9.6	9.6	5.6	5.6	5.6	5.6
	٨		10/16/74 5.6	10/16/74	25/17/01	10/23/74	10/23/74	10/23/74	10/23/74	10/23/74 5.6	10,725,774	10/25/74 5.6	10/25/74 5.6	10/25/74	10/25/74	10/25/74	10/25/74	10/25/74 5.6
	Table IV	P. (813)	185	210	585	185	210	235	582	335	10S	185	185	210	130	155	52	282
	Ta	POT PTT (PSIG) DATE	185	210	585	185	210	235	282	335	101	181	181	305	921	151	122	182
		PN2 (PS16)	1350	1732	1463	1350	1923	1129	1568	3601	2110	1350	1350	1923	1516	1839	5211	1568
		Noz	0.563	0.563	0.265	0.563	0.563	0.432	0.432	0.330	0.563	0.563	0.563	0.563	0.432	0.432	0.432	100 0.432
		200	5	5	28	100	5	100	100	ğ	2	100	8	100	2	23	55	8
		٠-٥	R	£	ı	g	Ž.	į	Î	ğ	1	Amb	£	£	Ą	2	2	£
		4	1	ę	ğ	200	500	200	200	8	2	ę	ş	2	1	2	£	1
SECRETARIA PA	CENT	TA	1.6	3.	1.6	1.6	1.6	1.6	1.6	9:	1.6	1.6	1.6	3.5	1.6	1.6	1.6	1.6
MAR	UA	"	8	12	95	55	521	150	002	8	501	3	8	MM 125	22	8	8	92
SELECT POOR		Fuel	ğ	\$	£	ğ	\$	2	8	8	ž	*	£	Ē	\$	£	ž	ğ
O.G.		5	525	020	.020	020	.020	.020	020.	8.	.020	020.	.020	020	020	.020	626.	020.
		Test Vo.	101-72-30	-132	H -	-134	-135	-136	-137	138	-139	-140	DA-	-142	297-	.18	-145	-145

FR/Rate Process W/2-X.D.F. REMARG	400 Push 1 Stop 14 Long Impingement . Element	Long Impingment Element	Long Jayingerent Element	tony Impingment Element	Long Impingement Element	Long Impingment Element
W/2-X-D.F.	Ħ.	Ħ	2	2	×	
Process	Push 1 Stop	400 Push 1 Stop 14	400 Push 1 Stop	400 Push 1 Stap	400 Push 1 Stop	200 Fush 1 Stop 14
FR/Rate (FPS)		600	8	400	8	7.00
(PSIG) (PSIG) (PSIG) DATE 1-Stop		5.6	5.5	5.6	5.5	9.6
DATE	100 0.330 1095 331 335 10/25/74 5.6	20 0.563 2110 101 105 10/25/74 5.6	0.563 1350 181 185 10/25/74 5.6	385 10/25/74 5.6	5.5 10/25/74 5.5	100 0.187 1463 1081 1085 10/25/74 5.6
(9216)	335	105	185	385	222	1065
(9154)	ä	101	181	132	55	1081
(93:6)	1095	2110	1350	0.330 1350	0.265 1463	1463
Noz Vez	0.330	0.563			0.265	0.187
0,	55	22	55	951	5	81
-0	1	1	Û	1	ğ	1
-	Ą	£	1	ğ	Ą	1
25	1.5	1.6	1.6	1.6	1.6	1.6
Fuel Pc NO	220	8	8	330	283	1000
Fue	Ē	ğ.	Ě	Š	\$	8
	. 920	020	623.	020.	.020	-152 .020
Test No. Or	00-27-147 .020	.143	-149	-150	-151	-152

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TABLE V - COMPUTER LISTING - TEST SUMMARY HIGH PERFORMANCE, N204 / AMINE ELEMENTS

HYPERGOLIC STREAM IMPINGMENT DATA COMPLIATION

INVESTIGATOR LAWVER

A L R C MODEL CORPELATION PARAMETERS

(PSIA)

FAF)

	AIG	(SEC)	.31-03	.30-03	.31-03	.31-03	.32-03	.29-03	.32-03	.32-03	.29-03	.31-03	.29-03	•52-03	.30-03	.33-03	.31-03	.34-03	.45-03	.31-03	.32-03	.31-03	.31-03	.36-03	.37-03	.39-03	-31-03	.33-03	50-67	.32-03	.29-03	.31-03	.30-03	.29-03	.55-01	.29-03	.29-03	.29-63	-25-03	.27-03	.68-03	.26-03
				*	*		*					*	*	*													2							*				*				
	COMMENTS		SEP	MIX	MIX	MIX	MIX	SEP	SEP	SEP	SEP	SEP	SEP	MIX	SEP	SEP	SEP	SEP	SEP	SEP	SEP	SEP	SEP	MIX	MIX	SEP	SEP	SEP	635	63S	d25	DINCEF	UNDEF									
	NE/NO		.875	.975	*908	.913	.629	.975	.832	*889	.889	.932	.926	*624	006*	.675	.378	.862	.888	.931	+06.	968.	.910	.876	.880	.913	.928	.953	696.	.951	056.	126.	\$96°	.958	.674	. 859	.873	• 595	*350	1-015	41.	* 922
	KIR.		1.65	1.57	1.62	1.62	1.70	1.57	1.70	1.65	1.64	1.60	1.60	1.59	1.63	1.56	1.65	1.67	1.64	1.60	1.64	1.63	1.62	1.65	1.65	1.61	1.60	1.59	1.53	1.58	1.60	1.56	1.57	1.58	1.66	1.74	1.72	1.74	1.74	1.00	1.45	1.61
	75	(F)	87.	87.	R7.	87.	38.	88.	85.	84.	84.	33.	83.	76.	67.	82.	78.	77.	76.	81.	82.	81.	80.	. 64	77.	82.	81.	82.	81.	83.	83.	82.	83.	83.	R3.	197.	.00.	1001	150.	195.	.05	.29
	10	(F)	88.	88.	.58	88.	89.	69.	86.	84.	84.	83.	84.	76.	88.	82.	81.	80.	78.	81.	82.	82.	81.	81.	77.	82.	83.	93.	84.	85.	85.	85.	85.	86.	. 20	77.	73.	77.	16.	19.	61.	£4.
	VF	F1/5)	29.	32.	23.	29.	25.	38.	24.	24	36.	9	35.	76.	32.	21.	50.	.00	88.	27.	24.	0	29.	. 40	68.	01.	30.	32.	80.	26.	35.	29.	33,	36.	79.	36.	39.	30.	143.8	48.	58.	*7
	vo	(FT/S) (07.	90	.90	55	67.		.90	03.	12.	104.6	.60	.09	08.	101.6	08.	99.	73.3	03.	02.	104.5	05.	86.	89.7	82.	105.5	05.	63.	01.	69.	02.	050	.80	60	10.	11.	10.	116.2	-	42.5	115.9
	2	PSIA)	308.	308.	309.	311.	507.	.000	308.	263.	197.	158.	100.	.68	101.	162.	203.	269.	301.	310.	510.	003.	100.	338.	334.	955.	495.	298.	283.	256.	191.	152.	95.	114.	4111.	. 25.	119.	150.	163.	243.	103.	61.
CAL	ANGLE	(030)	.09	.09	.09	.09	.09	50. 1		.09	.09	.09	.09	.09	.09	.09	.09	.09	.09	09	.09	60. 1		.09	.09	.09	60.	.09	.09	.09	.09	.09	.09	.09	.09	.09	-09	.09	.09	.09	.09	*09
	1,00		24.	24.	54.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	24.	٠42	.47	. 57	24.	24.	24.	24.	54.	54.	24.	24.	* 4.2	24.	.4.7		24.	. 5.7	24.	. 82
	35	(IN)	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	.020	070-	.020	.020	.020	.020	.020	.020.	.020	.020	070*	.020	.020	.020	.020
	00	1110	022	022	022	022	022	022	.022	322	022	022	022	022	022	025	922	022	022	022	022	.022	022	022	022	022	025	325	022	320	250	025	-022	220	220	.022	.022	1022	220	.022	.022	.022
	EST	NO.																																					137			
		Type	MAN	MANN	MAM	MAH	XXH	MVH	Hox	MXM	HXW	WIN.	K:H	A-5.	4-50	A-50	A-50	A-50	A-50	A-50	4-5u	A-50	4-50	A-50	4-50	MMM	MHH	HAM	MXH	MNH	Жин	HAN	HXXH	HNH	H.X	HON	MAK	HAM	T. T.	HAH	HZW	HAS.
												-	20)-						1										2												

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HIGH PEPFORMANCE N204 / AMINE ELEMENTS

HIPE-GOLIC STREAM IMPINGMENT DATA COMPLIATION

FUEL TEST DO DF L/D ANGLE PC VO VF TO TF MR NF/NO COMM FUEL TEST DO DF L/D ANGLE PC VO VF TO TF MR NF/NO COMM FUEL TEST DO DF L/D ANGLE PC VO VF TO TF MR NF/NO COMM WHH 141 1022 1020 24. 60. 81. 115.2 145.2 66. 64. 1.60 .935 UND WHH 141 1022 1020 24. 60. 119. 106.7 186. 67. 1.59 .958 WHH 141 1022 1020 24. 60. 119. 106.7 186. 67. 1.59 .958 WHH 141 1022 1020 24. 60. 119. 106.7 186. 67. 1.53 1.026 WHH 144 1022 1020 24. 60. 129. 38.6 54.2 67. 67. 1.53 1.026 WHH 145 1022 1020 24. 60. 129. 135.9 68. 67. 1.62 .908 WHH 146 1022 1020 24. 60. 129. 109.7 184.2 68. 67. 1.51 1.92 WHH 149 1022 1020 24. 60. 293 100.7 184.2 68. 67. 1.51 1.92 WHH 149 1022 1020 24. 60. 293 100.7 184.2 68. 67. 1.51 1.92 WHH 149 1022 1020 24. 60. 293 100.7 184.2 68. 67. 1.51 1.92 WHH 155 1022 1020 24. 60. 893 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 22. 020 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 22. 020 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 22. 020 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 22. 020 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 22. 020 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 1.62 .912 SERVAN 155 1022 24. 60. 998 121.1 146.3 78. 74. 146. 146. 146. 146. 146. 146. 146. 14	Page 2 of 2	IT DATA COMPLIATION	A L R C MODEL CORPELATION PARAMETERS	COMMENTS * DIV FWF Dre (PCIA)	* .28-03 .00	* .29-03	UNDEF73-03 .00	• • • • • • • • • • • • • • • • • • • •	* .31-03	* .29-03	* .32-03 .00	• • • • • • • • • • • • • • • • • • • •	* .30-03	* .30-03 .00	• • • • • • • • • • • • • • • • • • • •	* .27-03 .00	
2		STREAM	LAWVER	VF TO TF WR	2 143.2 66. 64. 1.60	7 136.7 68. 67. 1.59	6 54.2 67. 67. 1.42	8 55,7 67, 67, 1.53	9 128.4 66. 67. 1.62	5 135.9 68. 67. 1.57	7 124.2 68. 67. 1.61	1 58.8 68. 68. 1.49	7 133.6 69. 69. 1.69	2 131.9 70. 69. 1.52	5 137.8 70. 69. 1.64	78. 74. 1.62	
			GE IS	DO DF L/D ANGLE PC (IN) (IN) (DEG) (PSIA)	.022 .020 24. 60. 81.	.022 .020 24. 60. 119.	.022 .020 24. 60. 129.	.022 .020 24. 60. 154.	.022 .020 24. 50. 152.	.022 .020 24. 60. 190.	.022 .020 24. 60. 258.	.522 .020 24. 60. 102.	.022 .020 24. 60. 99.	.022 .020 24, 60, 297.	.022 .020 24. 60. 484.	.022 .020 24. 60.	Contain and categories and a rest

S9 LINES ZETA PLOT FILE IRSSSS142152 CONTAINS

NISS

TABLE VI HIGH PRESSURE RSS LIMITS

Fuel	Predicted Limit	Measured Limit
N2H4	300	300
ММН	400	150
A-50	500	200

TABLE VII

COMPARISON OF HEAT RELEASE RATES AND RSS LIMIT

<u>Fuel</u>	P _V (psia) at 100°F	Heat Release Rate Kcal/sec-mole of NTO	Sep. Limit	
N ₂ H ₄	0.65	4 x 10 ⁴	300	
A-50	4.6	e la	200	
UDMH	11.0	14 x 10 ⁴		
ммн	2.1	20 x 10 ⁴	150	

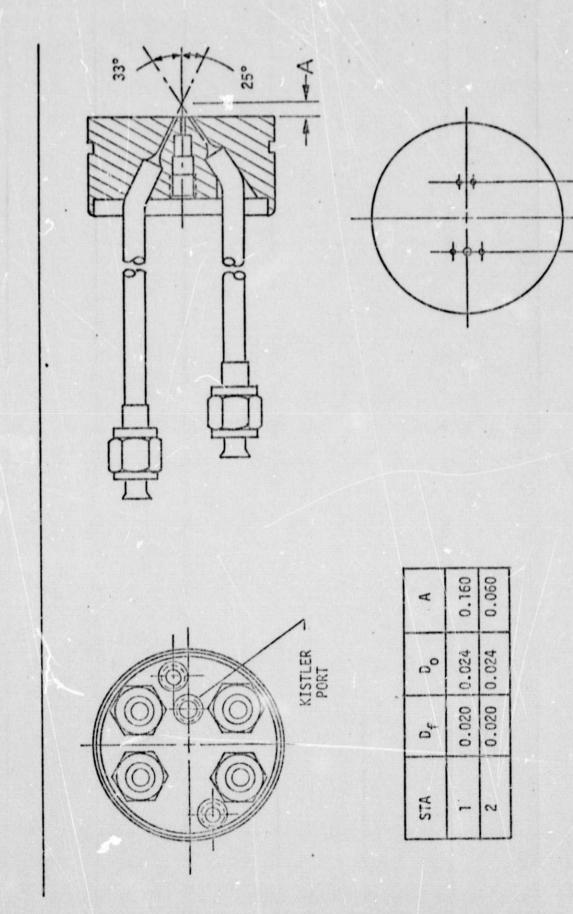
TABLE VIII
HIGH FREQUENCY RESPONSE INSTRUMENTATION

Test Parameter	Symbol	Instrument Make	Model	Range	Accuracy
Oxidizer Manifold Pressure	POJHF	Kistler	601	0-3000 psi (P-P)	± 0.5%
Fuel Manifold Pressure	PFJHF	Kistler	601	0-3000 psi (P-P)	± 0.5%
Chamber Pressure	PCHF	Kistler	601	0-3000 psi (P-P)	+ 0.5%
Injector Acceleration	ACC			0-500 g's	± 0.5%
Injector Probe Temperature	TP1	C/A		0-500 °F	± 1%

TABLE IX
LOW FREQUENCY RESPONSE INSTRUMENTATION

	SYMBOL	RANGE	UNITS	RECORDER		
TEST PARAMETER				"O" GRAPH	TAPE	DIGITAL
Oxid. Tank Pressure	POT	0-1500	PSIA	X		
Fuel Tank Pressure	PFT	0-1500	PSIA	X		
Oxid. Injector Pressure	POJ	0-1500	PSIA	X		X
Fuel Injector Pressure	PFJ	0-1500	PSIA	X		X
Chamber Pressure	PC	0-1000	PSIA	X		X
Window Purge Pressure	PNZ	0-2000	PSIA	Χ .		x
Oxid. Flowrate	WO	0-0.1	LB/SEC	X		X
Fuel Flowrate .	WF	0-0.1	LB/SEC	X		X
Oxid. Flowmeter Temp.	TOFM	0-500	o _F	x		. x
Fuel Flowmeter Temp.	TFFM	0-500	oF	Х		Х
Oxid. Injector Temp.	TOJ	0-500	o _F	X		
Fuel Injector Temp.	TFJ	0-500	o _F	x		
Oxid. Valve Voltage	VOV			x		
Fuel Valve Voltage	VFW			/ x		
Wind Purge Valve Voltage	VWPV			X		
Camera Voltage	VCAM			Х	X	
Injector Purge Valve Voltage	VIPV			X		

Unite Doublet Injector



STA (2)

STA (1)

FIGURE 1. UNLIKE DOUBLET INJECTOR

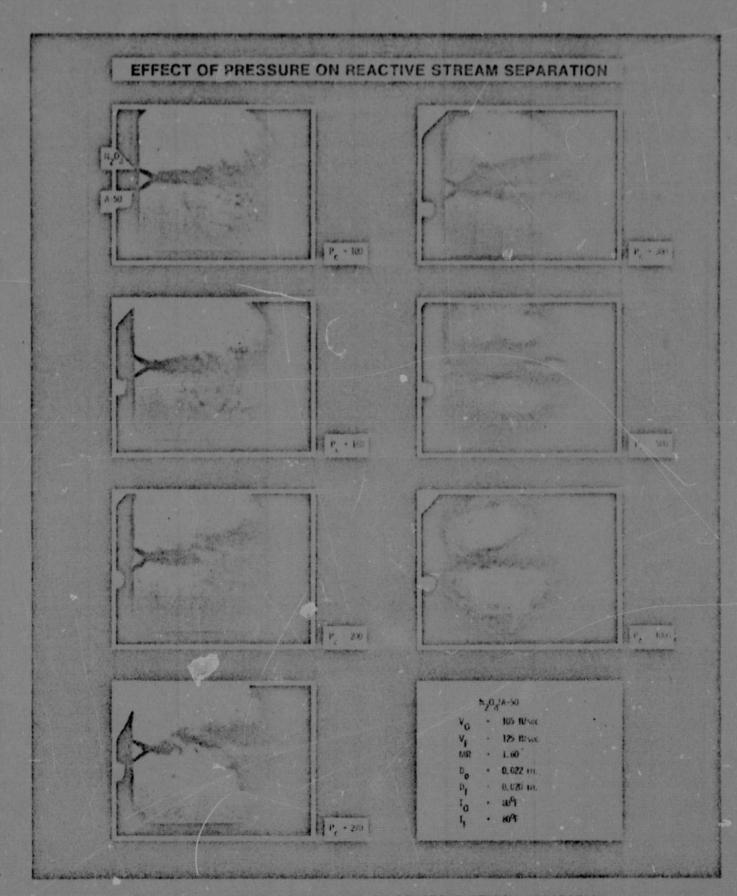
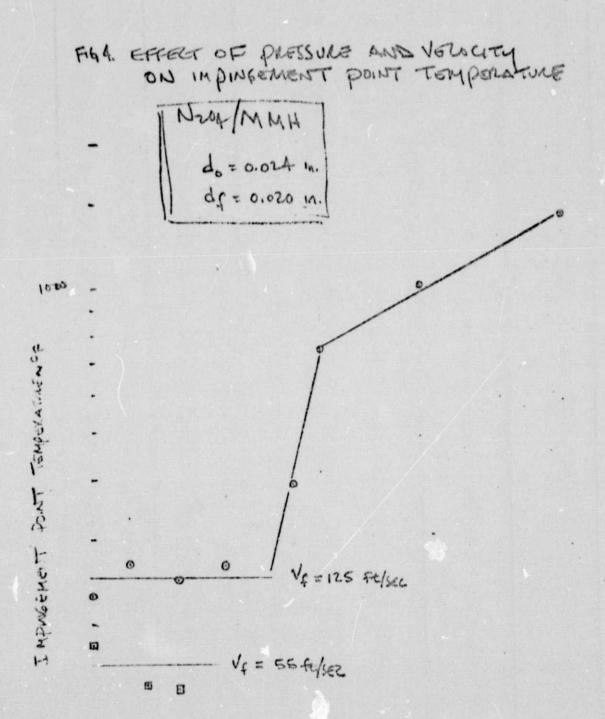


FIGURE 2. EFFECT OF PRESSURE ON REACTIVE STREAM SEPARATION

EFFECT OF TEMPERATURE ON REACTIVE STREAM SEPARATION T, - 70% T, - 200°F MONH / N204/MMH . 105 ft/sec - 125 ft/sec - C. 024 in. THERMOCO IPLE - 0.020 In. - 70°F



100 100

CHAMBER PREISURE N PSIA -28-

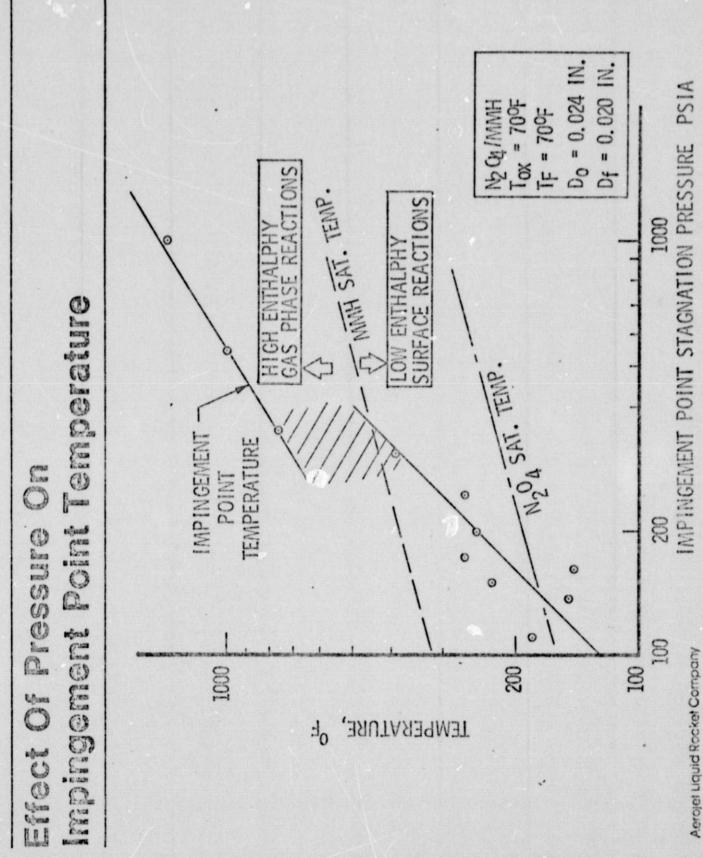


FIGURE 5. EFFECT OF PRESSURE ON IMPINGEMENT POINT TEMPERATURE

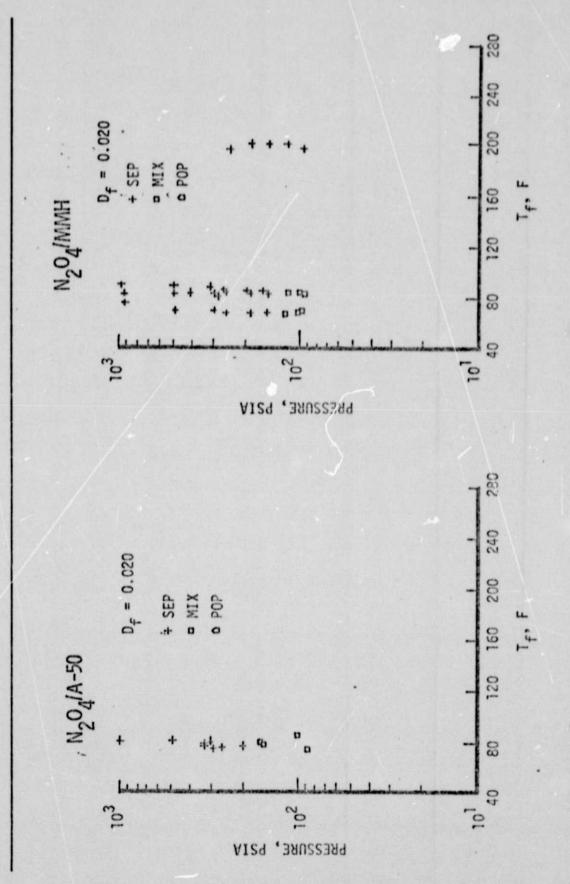


FIGURE 6. EFFECT OF PRESSURE AND TEMPERATURE ON RSS

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Task I - Model & Data Review Data Plots

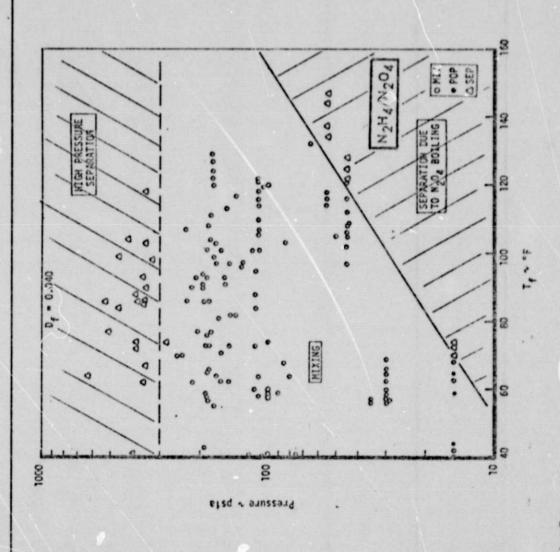


FIGURE 7. TASK I - DATA PLOT

Postulated RSS And Controlling Mechanisms

POPPING REGIME MIXING REGIME DIFFUSION -DECOMPOSITION DIFFUSION FLAME DIFFUSION REACTION FLAME OR SURFACE SURFACE N204 HYPERGOLIC HEATING

VAPOR PHASE REACTION CONTROLLED

- HIGHER PRESSURE
- SMALLER ORIFICE DIAMETER
 - LOWER PROPELLANT TEMP.

SURFACE REACTION CONTROLLED

- LOWER PRESSURE
- LARGER ORIFICE DIAMETER
 - LOWER TEMP.

N2 O4 VAPOR PRESSURE CONTROLLED LOW PRESSURE SEPARATION REGIME

- LOWER PRESSURE
 - . HIGHER TEMP.

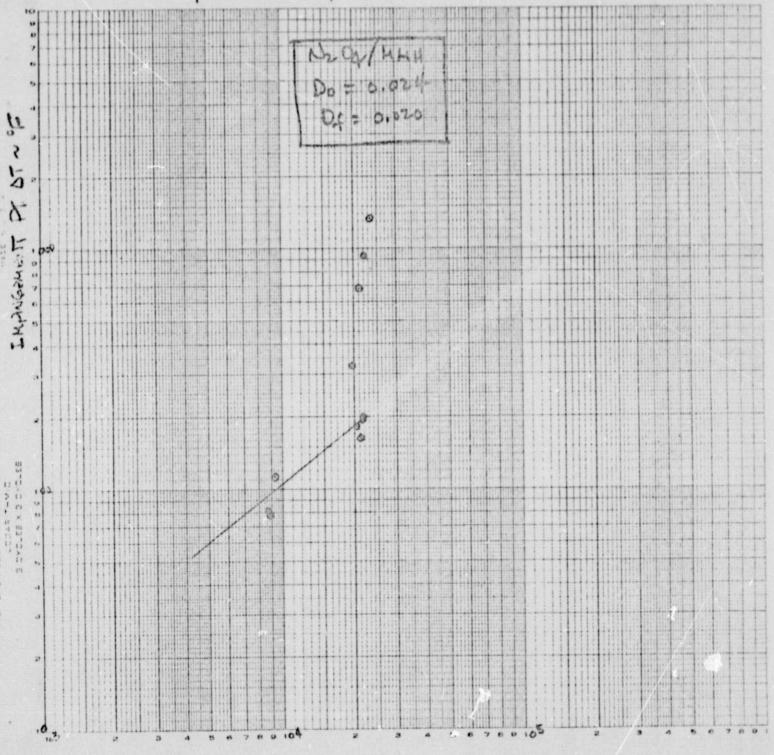
HIGH PRESSURE SEPARATION REGIME

MONOPROPELLANT DECOMPOSITION CONTROLLED

* HIGHER PRESSURE

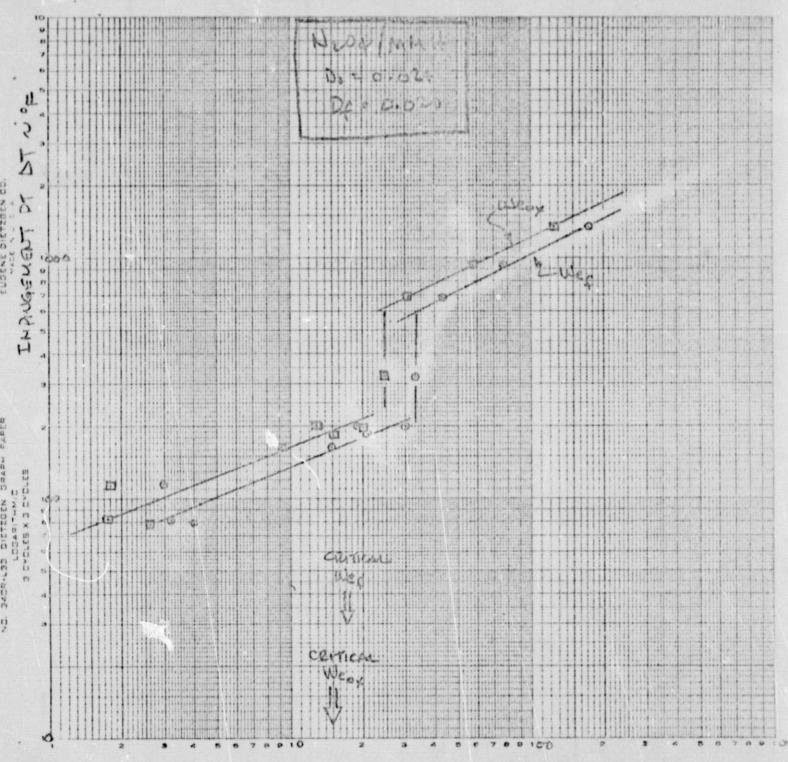
Cerojet Liquid Rocket Company

FIG9-EFFECT OF REYNOLDS NO. ON IMPINGEMENT POINT TEMPERATING RUSE



FUEL REGINOLOS NO. ~ PVZ

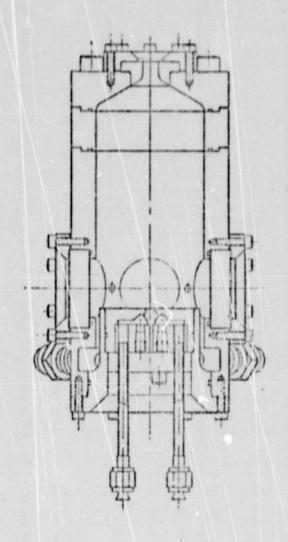
FIG.10-EFFECT OF WEBER NO. ON IMPINGEMENT PT. TEMPERATURE BASE



WESER No. ~ PAVEd

Aerojet Liquid Rocket Company

Definition of Governing Mechanisms Fabrication FORTING POLICE EXTERNO Design 000



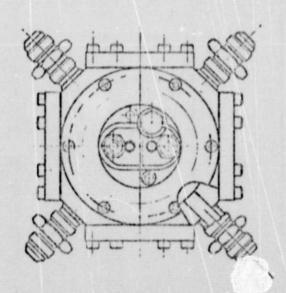


FIGURE 11. TASK III . TEST CHAMBER

Task III - Definition Of Governing Mechanisms Photographic Setup

1000 WATT QUARTZ/10DINE

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HYCAM HIGH SPEED CAMERA

TEST CHAMBER

Aerojet Liquid Rocket Company

FIGURE 13. TASK III - PHOTOGRAPHIC SETUP

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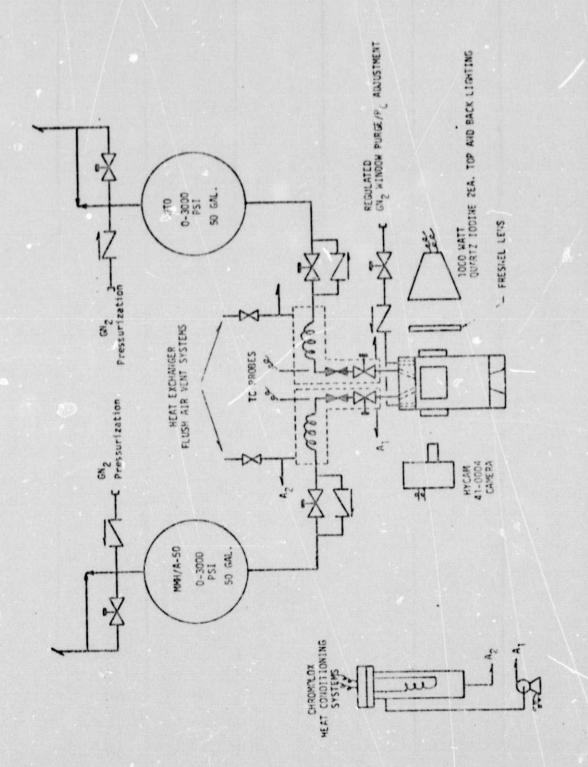
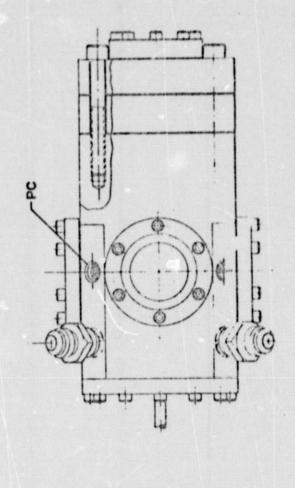


Figure 14. Propellant Flow System Schematic



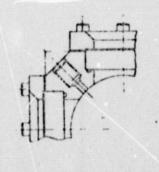


Figure 15. Instrumentation Schematic